Amendments to the Claims:

This listing of claims will replace all prior versions and listing of claims in the application.

Listing of Claims:

- 1-5. Cancelled.
- 6. (Currently Amended) A process for preparing a 2-(chloromethyl) phenylacetic acid derivative of formula I,

where X is C1-C4-alkoxy or methylamino,

said process comprising ether cleaving by ether cleavage a compound of formula II,

where R is C1-C4-alkyl, C1-C4-alkoxy, C1-C2-haloalkyl, C1-C4-alkylcarbonyl, C1-C4-alkylcarbonyloxy, halogen, nitro or cyano and X is as defined above, with hydrogen chloride, in the presence of an inert solvent and a catalyst. wherein said catalyst is selected from the group consisting of iron, indium and halides, oxides and triflates thereof.

- 7. (Canceled)
- 8. (Previously presented) The process of claim 6, wherein said catalyst is iron (III) chloride.
- 9. (Previously presented) The process of claim 6, wherein said catalyst is iron.
- 10. (Previously presented) The process of claim 6, wherein said catalyst is indium (III) chloride.
- 11. (Previously presented) The process of claim 6, wherein said catalyst is iron (III) oxide.
- 12. (Previously presented) The process of claim 6, wherein said catalyst has a concentration in the components of the ether cleaving reaction of about 0.001 to 0.5

mol equivalents.

- 13. (Previously presented) The process of claim 6, wherein said catalyst has a concentration in the components of the ether cleaving reaction of about 0.01 to 0.2 mol equivalents.
- 14. (Previously presented) The process of claim 6, wherein said hydrogen chloride has a concentration in the components of the ether cleaving reaction of about 1 to 25 mol equivalents.
- 15. (Previously presented) The process of claim 6, wherein said hydrogen chloride has a concentration in the components of the ether cleaving reaction of about 1 to 10 mol equivalents.
- 16. (Previously presented) The process of claim 6, wherein said hydrogen chloride has a concentration in the components of the ether cleaving reaction of about 3 to 5 mol equivalents.
- 17. (Previously presented) The process of claim 6, wherein said inert solvent is an aromatic hydrocarbon.

- 18. (Previously presented) The process of claim 6, wherein said inert solvent is an aliphatic (halogenated) hydrocarbon.
- 19. (Previously presented) The process of claim 6 wherein said hydrogen chloride is passed into the ether cleaving reaction mixture in gaseous form.
- 20. (Previously presented) The process of claim 6 wherein said hydrogen chloride is condensed into said ether cleaving reaction.
- 21. (Previously presented) The process of claim 6 further comprising adding at least one Lewis base to the said ether cleaving reaction.
- 22. (Previously presented) The process of claim 16 wherein said Lewis base is pyridine.
- 23. (Previously presented) The process of claim 16 wherein said Lewis base is N,N-dimethylaniline.
- 24. (Previously presented) The process of claim 16 wherein said Lewis base is ethanethiol.

- 25. (Previously presented) The process of claim 6 further comprising adding trimethylsilyl chloride to said ether cleaving reaction.
- 26. (Currently Amended) The process of claim 6 further comprising conducting said ether cleaving reaction in a biphasic system in the presence of a phase transfer catalyst—, wherein the phase transfer catalyst is selected from the group consisting of tetrabutylammonium chloride, tetrahexylammonium chloride, tetrabutylphosphonium chloride, bis(triphenylphosphoranylidene) ammonium chloride, trimethylbenzylammonium chloride, triethylbenzylammonium chloride and triphenylbenzylammonium chloride.
- 27. (Previously presented) The process of claim 6 further comprising performing said ether cleaving reaction under a protective gas atmosphere.
- 28. (Previously presented) The process of claim 6 wherein said ether cleaving reaction temperature is between about 0 to 100°C.
- 29. (Previously presented) The process of claim 6 wherein said ether cleaving reaction temperature is between about 30 to 70°C.
- 30. (Previously presented) The process of claim 6 wherein said ether cleaving reaction

pressure is from about 0 to 6 bar.

31. (Previously presented) The process of claim 6 wherein said ether cleaving reaction pressure is atmospheric pressure.